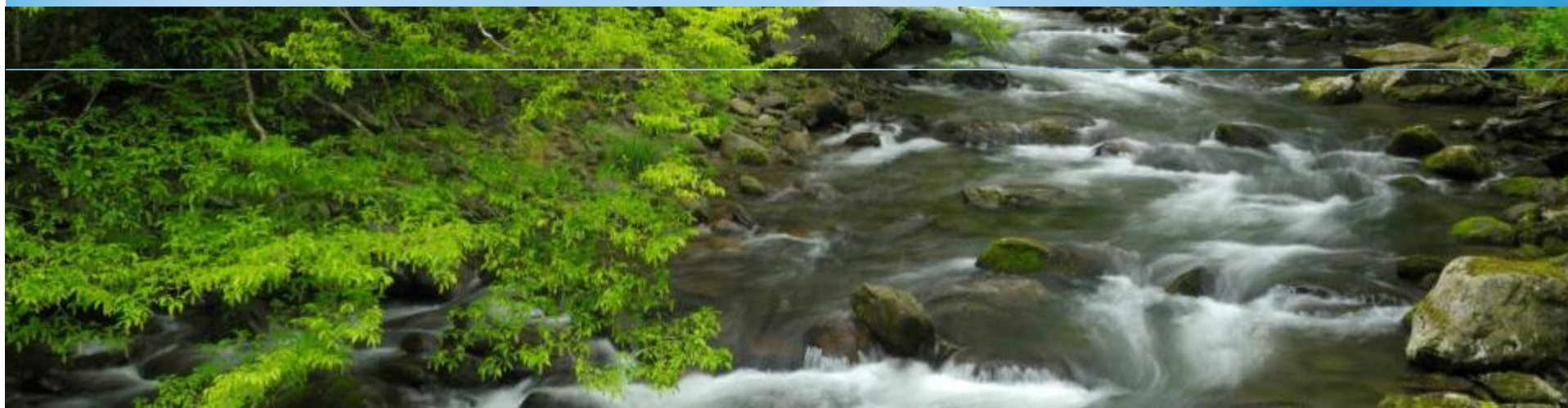




Innovative Ion Exchange Solutions for Small Community Nitrate Treatment Systems

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Envirogen Technologies, Inc.



Nitrate Treatment Technology Workshop

5 September 2013

Topics we will cover

- Small system design challenges
 - Process considerations
 - Operational issues
- MinX product line
 - Systems in operation w/
performance summary
 - Nitrate Pilot results
- Case Study– CAPEX and OPEX costs
- Options for other contaminants

Small system design challenges

- Process considerations
 - Flow Rate, Peak/ Average vs. Reality
 - Influent WQ variability
 - System Utilization/ Availability
 - Treatment Goal, System vs. Overall
 - Waste Rate- 40% to 60% of OPEX

Small System Design Challenges

- Operational issues
 - Resources
 - Personnel
 - Financial
 - Infrastructure limits
 - Well pump and controls
 - Facility
 - Utilities
- Long term operation
 - Technical support
 - Process improvements
 - Changing regulations

Envirogen IX Systems-Smaller Flows

- MinX™
 - 20– 500 GPM
 - Regenerable IX system
 - Simplified SimPACK design for smaller applications
 - Indoor applications - i.e., well pump houses
- MinFlex™
 - 5–25 GPM capacity
 - Regenerable iX system
 - Low utilization, limited process control
- FlexSorb™
 - Classic service exchange business
 - Typically less than 100 GP.
 - High BV applications
 - Intermittent use
- CleanPoint™

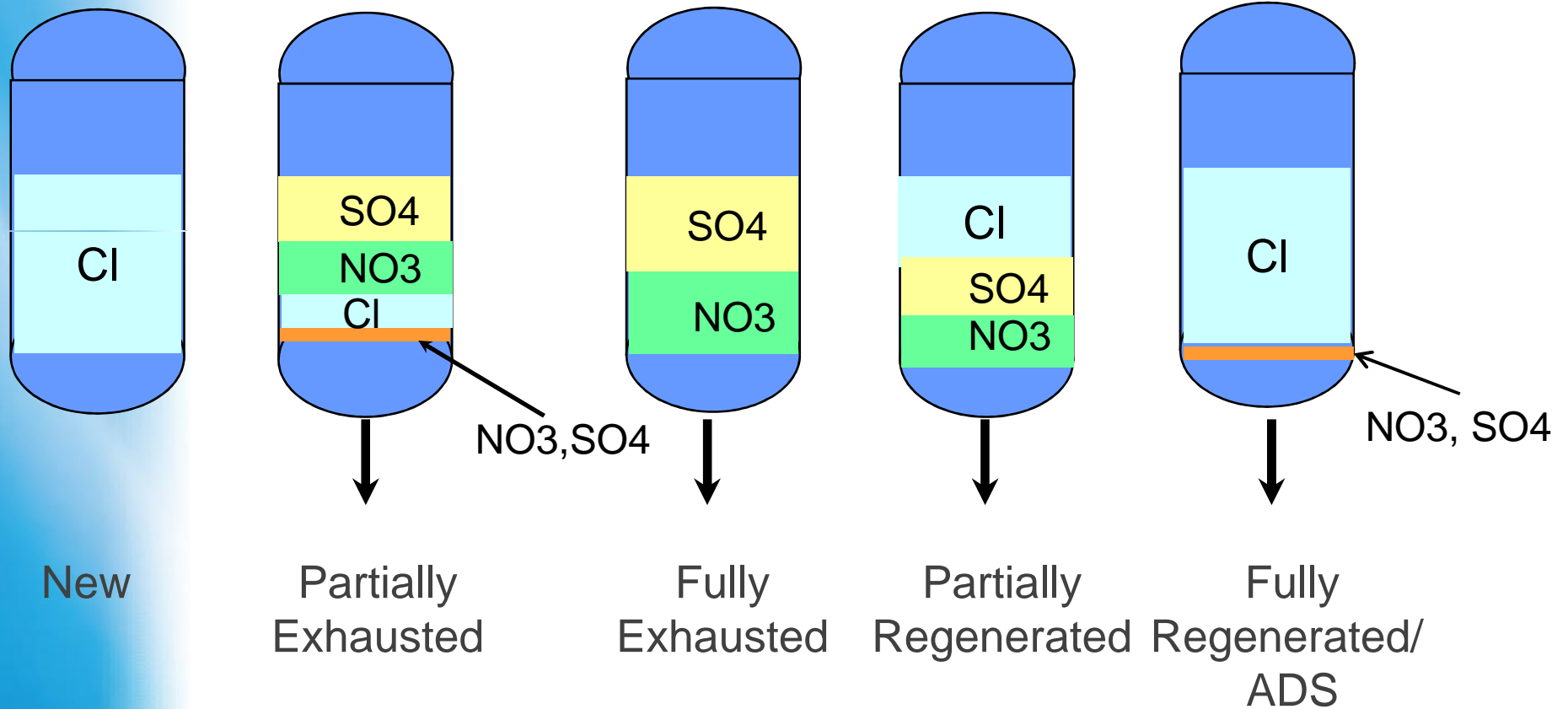


Regenerable Ion Exchange System Design

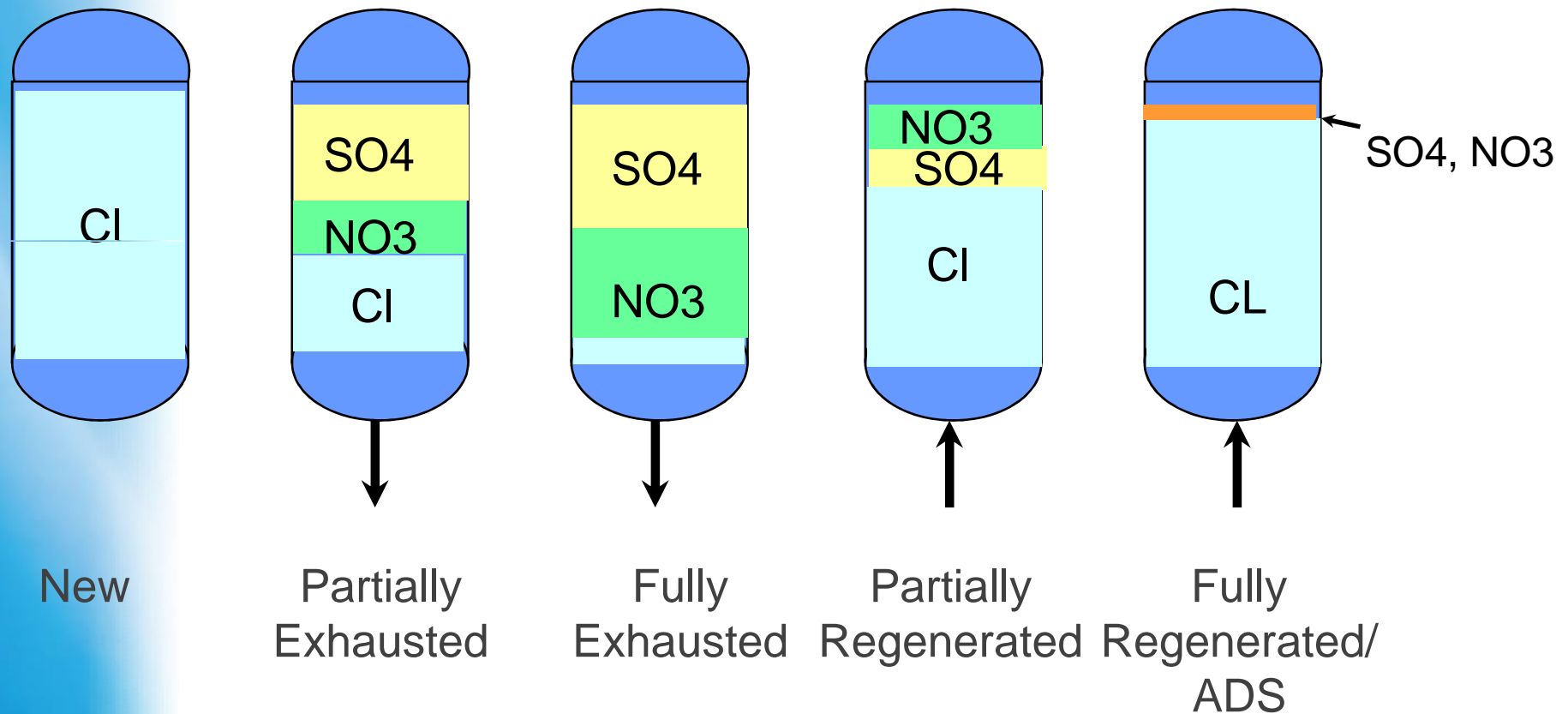
Recommended design basis- MinX

- Counter current regeneration- low NO_3 leakage
- Staggered (multiple) iX vessels, N+1 (N in service) - Internal Blending
- Two step brining process- Enhanced salt efficiency
- Water and brine recovery- minimize waste

Downflow – Co-current Regeneration

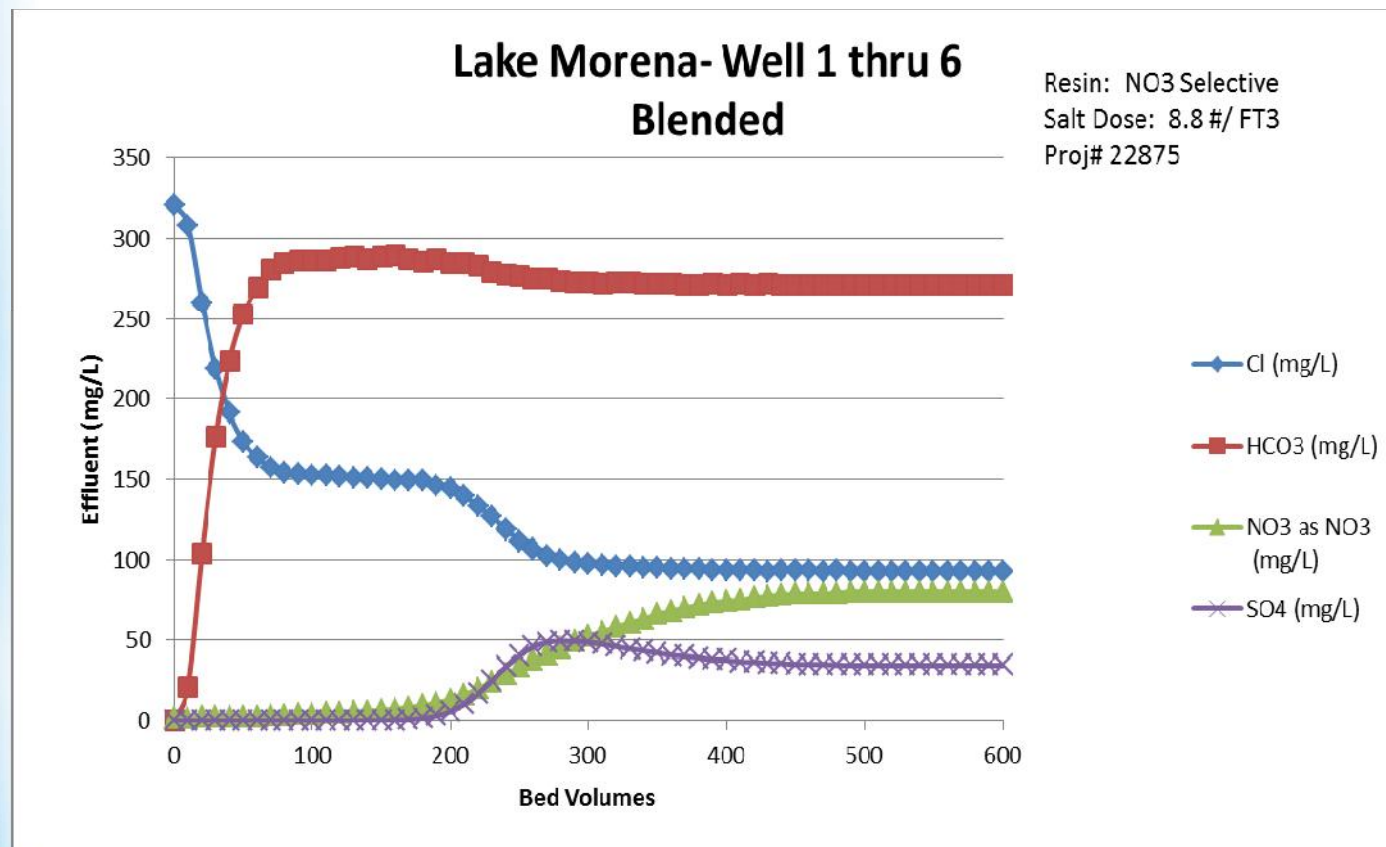


Packed Bed Counter-current Regeneration



Plug flow in both directions maintains wave front

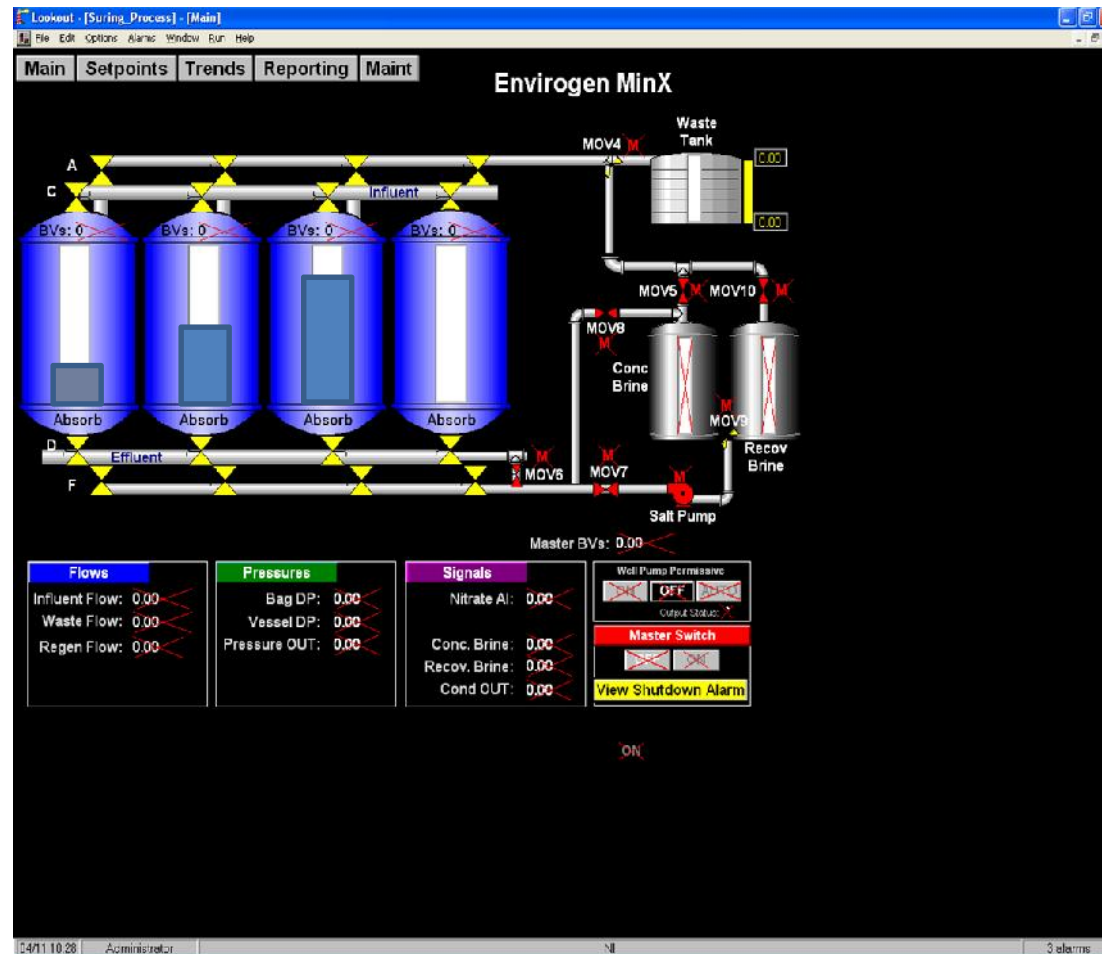
Single Bed Breakthrough



Staggered Bed Design- N=3

Influent NO3 (mg/L)	80.0			
NO3 Goal (mg/L)	36.0			
BV Set Point	445			
Vessels on line	3			
BV Waste	2.2			
BV Separation	148.3333333			
Vessel #	1	2	3	4
BV	445	296.6667	148.3333	0
NO3 Contrib	52.16804	49.13996	6.24712	1.61758
MAX Effluent NO3 (mg/L)	35.85			
Goal Met	Goal Met			
Waste Rate (%)	0.49%			
Goal Met	Yes			

MinX Process Controller



MinX Alarm Page



Lockout [Surfing_Process] [Alarm Setpoints]

File Edit Options Alarms Window Run Help

Main Alarm Setpoints Shutdown Reset

Feed Flow Hi:	0.0	OK	ENABLED	Delay:	0.0 s.
Feed Flow Lo:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Conc. Brine Level:	0.0	OK	ENABLED	Delay:	0.0 s.
Low Conc. Brine Level:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Rec. Brine Level:	0.0	OK	ENABLED	Delay:	0.0 s.
Low Rec. Brine Level:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Nitrate:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Hi Nitrate:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Regen Flow:	0.0	OK	ENABLED	Delay:	0.0 s.
Lo Regen Flow:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Waste Sump Level:		OK	ENABLED		
Hi Bag DP:	0.0	OK	ENABLED		
Hi IX DP:	0.0	OK	ENABLED	Delay:	0.0 s.
Hi Effluent Conductivity:	0.0	OK	ENABLED	Delay:	0.0 s.
Instrument Signal Fault:		OK	ENABLED		

04/11 10:33 Administrator NI 3 alarms

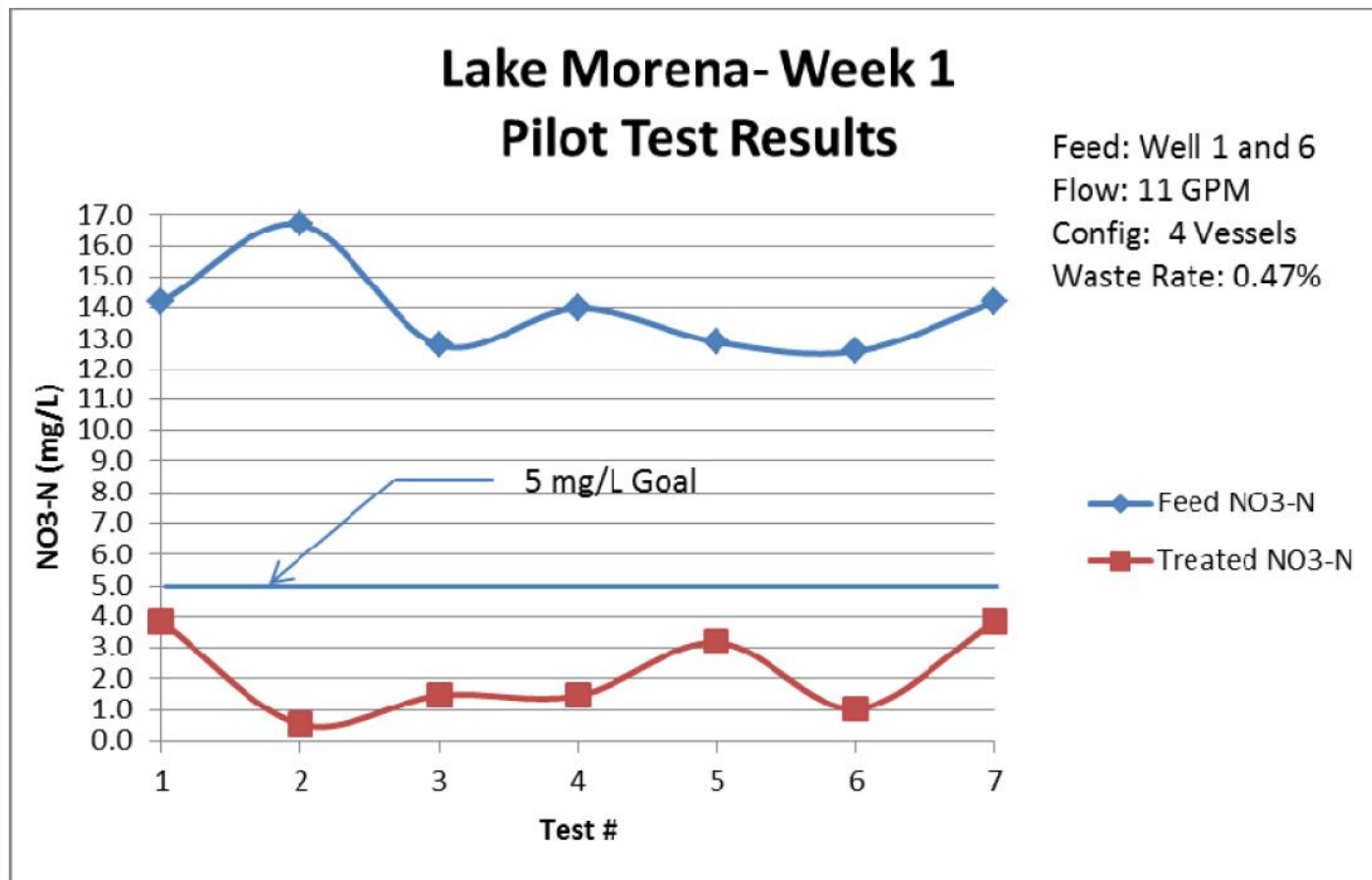
MinX System's Summary

- WI installation 1- 2010 Startup
 - Flow 350 GPM
 - NO₃-N, Influent- 10.3 mg/L, Effluent- 3.0 mg/L
 - Waste Rate 0.51%
- WI installation 2- 2011 Startup
 - Flow 265 GPM
 - Arsenic, Influent- 12 µg/L, Effluent- <4 µg/L
 - Waste Rate 0.08%
- KS Installation- 2013 Startup (300 GPM- NO₃)
- Lake Morena Oak Shores MWC- Pilot phase
 - Design Flow 50 GPM

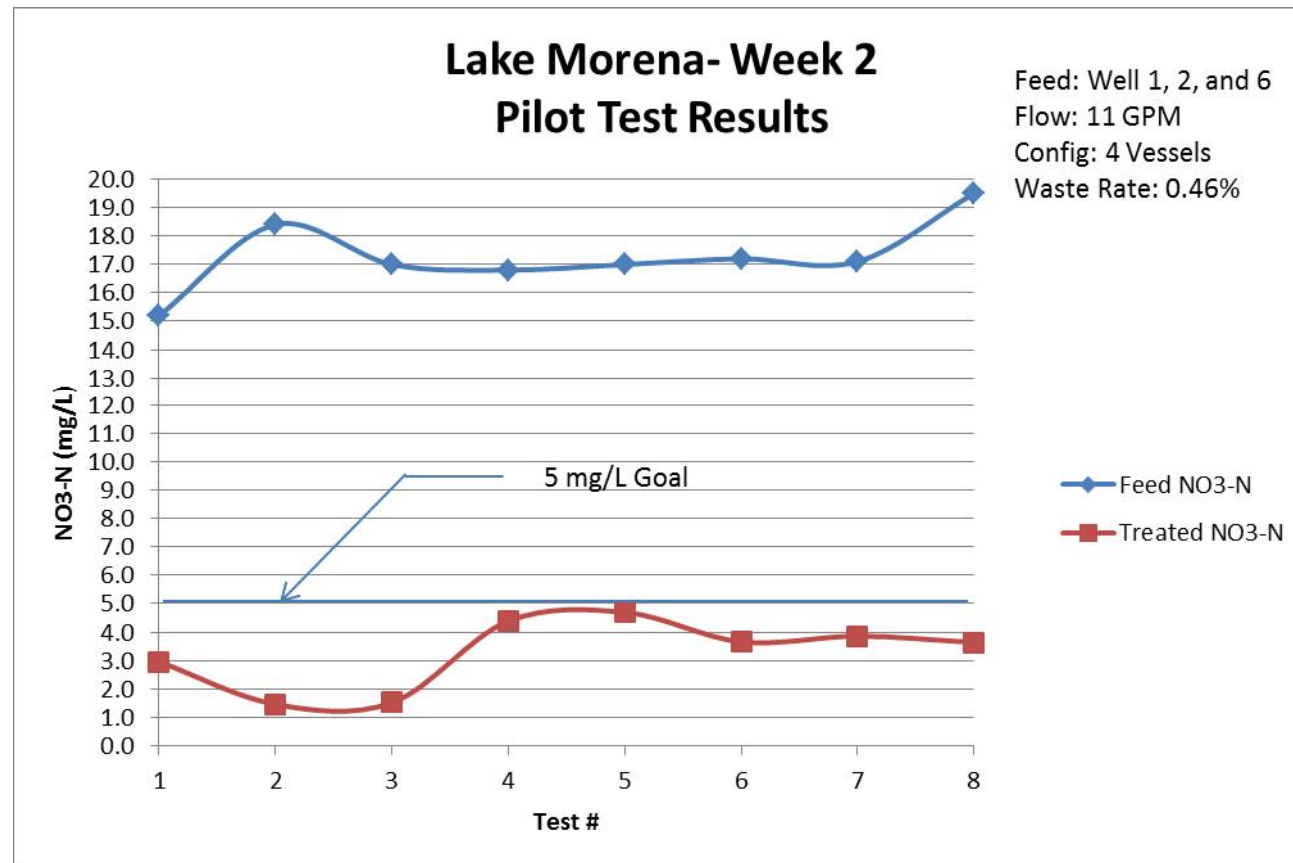
Lake Morena's Oak Shores MWC

- 50 GPM Capacity
 - 200 connection
 - 5 wells, 5 -18 GPM capacity
 - Influent NO₃-N, 12 - 23 mg/L
 - Well #5- Uranium at 40 pCi/L \pm 40 pCi/L
 - Treatment Goal, <5 mg/L NO₃-N
- Pilot Test
 - 4 week test
 - Goals
 - NO₃-N <5 mg/L
 - Waste rate <0.5% for Nitrate feed 9 mg/L
 - Waste rate <1.2% for Nitrate feed between 9 and 25 mg/L

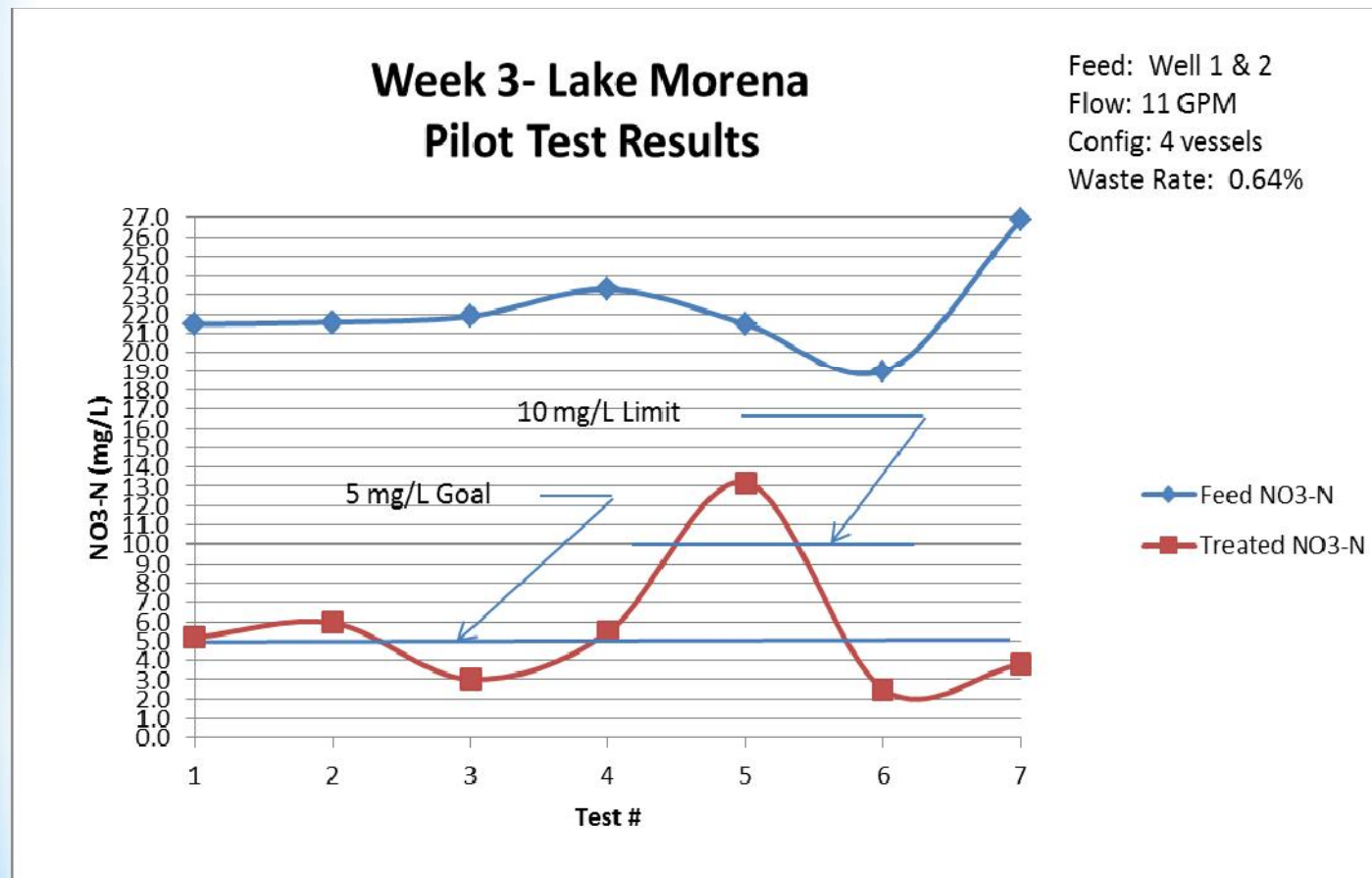
Pilot Test Results



Pilot Test Results



Pilot Test Results



T-6 Pilot Trailer



T-6 Pilot Trailer



Cost Summary- Case Study

- MinX capable of treating 125 GPM
 - No bypass required
 - 4 X Ø30" with 42" of media depth
 - N+1, 3 vessels on line, 1 vessel in regeneration/standby
 - Staggered bed design, counter current regeneration
 - Brine and water recovery
 - NO₃ analyzer, Post chlorination
- Process Conditions
 - BV Adsorption Set Point- 475 BV
 - Salt dose- 8 lb/ cf
 - Waste Rate- 0.48%, 12% NaCl concentration
 - Salt demand- 2.4 lb/ Kgal processed

Cost Summary- Case Study (Con't)

- Cost basis
 - Salt \$125/ ton delivered
 - Waste Disposal \$0.15/ gallon
 - Bag Filters \$3/ bag
 - Labor \$65/ hour, O/M
- Exclusions
 - Permitting costs
 - SCADA system

Cost Summary- Case Study

Description	Range
CAPEX	\$375K - \$438K
Equipment	\$150K - \$175K
Installation*	\$150K - \$175K
Engineering*	\$75K - \$88K
OPEX (Per MG treated)	\$918 - \$1,040

* Costs based on TDP capital factors

CleanPoint POE Treatment Systems

- Flow rate- 5 to 30 GPM
- Single use replaceable resin
 - Cr VI, As, ClO₄, U
- Lead-lag configuration
- PLC control
- 500 gallon internal storage tank
- Pre-filtration, post chlorination unit
- Optional RF telemetry package

CleanPoint 10C (Flexsorb)



Conclusions

- MinX provides, reliable, cost effective contaminant (ionic species) treatment for smaller feed flows
- Operational factors are critical in the treatment decision process
- Regenerable resin (i.e. NO_3 and As) systems– Waste disposal is largest operation costs
- Replaceable resin systems– Good for small flow rates, intermittent use, and contaminants with long bed life.



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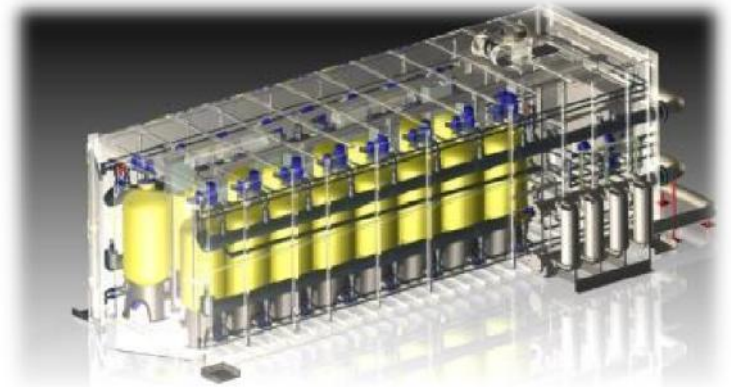
QUESTIONS?

How we do it...

SimPACK™ Ion Exchange

Advantages of SimPACK multi-bed vs. conventional ion exchange

- Flows greater than 300 gpm
- Off-site regeneration is not feasible/desired and the customer wants/needs to minimize the waste volume (0.05%- 2% vs. 2% - 6% for competitors).
- Patented counter-current, cascading, two-vessel regeneration process.
- Small footprint, rapid deployment
- Reduction in salt consumption



Three-Step Process

Treat (exhaust)
Regenerate (on-site)
Rinse

SimPACK Design

- Resin is regenerated on site
- Long-life resins
- The regeneration process is very rapid
- Multiple contaminants can be removed- “Long Term” View
- Robust and proven technology



Containerized SimPACK™ System

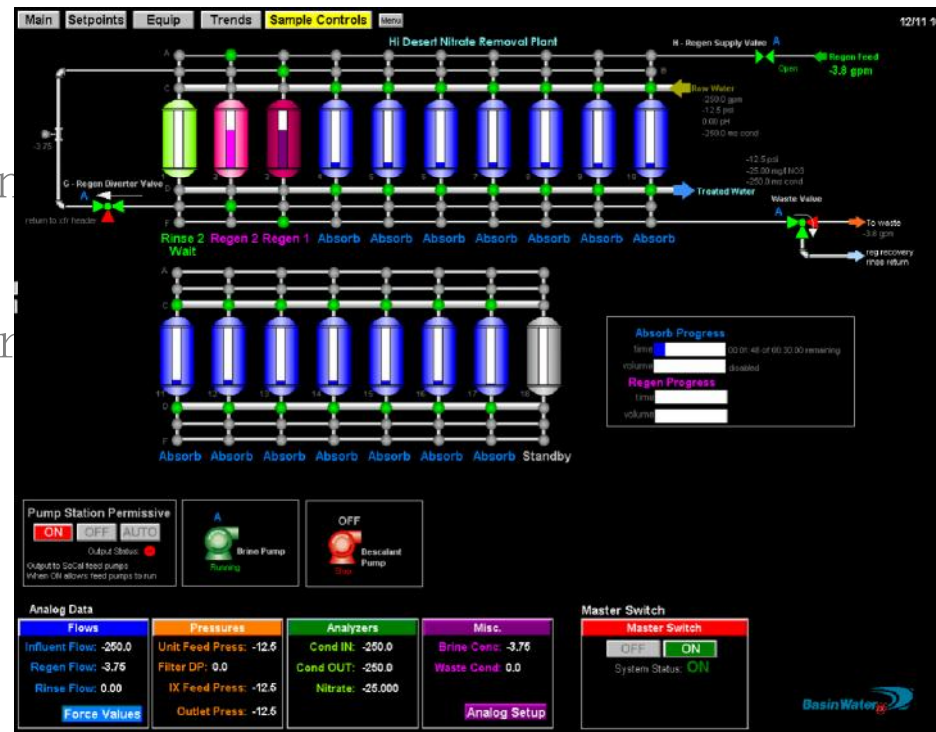


Process Control

SimPACK™ Ion Exchange

Multi-bed design generates lower waste

- Staggered bed design
- Maximize bed volumes
- Consistent blending design
- Minimize brine waste
- Reuse of final rinse water
- Data logging capabilities
- Built-in redundancy
- PLC process controlled
- 24/7 Telemetry



What we treat...

Nitrate Removal Systems



1,000-GPM Nitrate Removal System - California



2,000-GPM Nitrate Removal System - California

What we treat...

Uranium Removal Systems



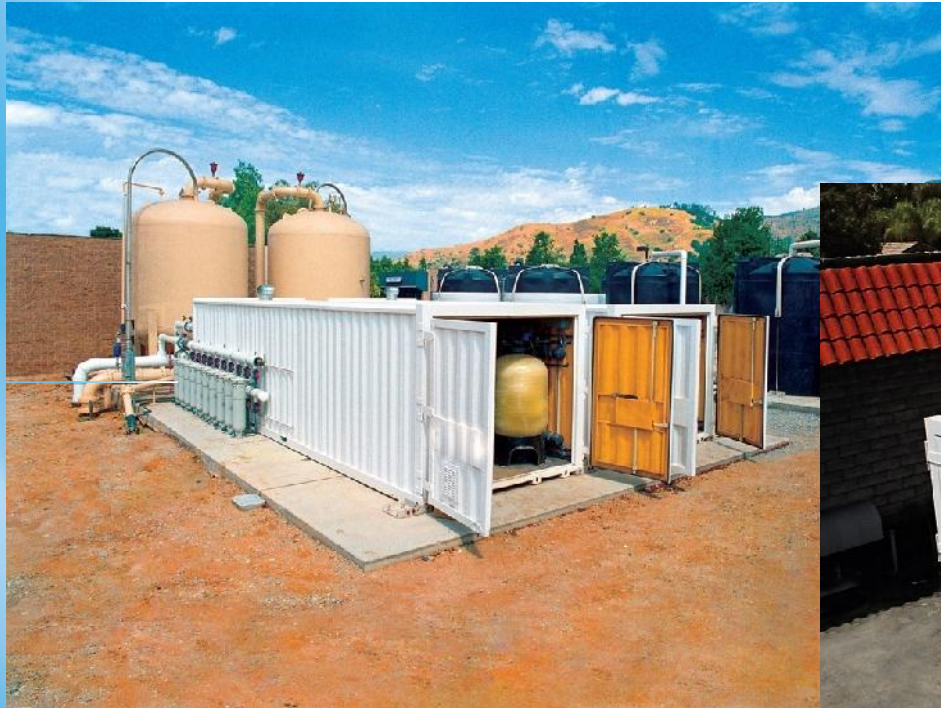
1,000-GPM Uranium Removal System - California



300-GPM Uranium Removal System - California

What we treat...

Perchlorate Removal Systems



2,000-GPM Perchlorate Removal System - California



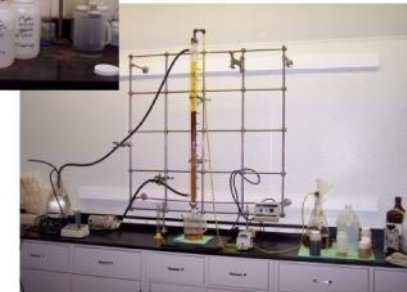
1,000-GPM Perchlorate Removal System - California

Laboratory & Pilot Capabilities

- Current staff has 50+ years of industrial chemistry, laboratory and pilot experience
- Analytical equipment includes Graphite Furnace AA, Flame AA and Ion Chromatograph
- Wet chemistry capabilities include standard procedures and specific tests that relate to ion exchange evaluations
- Small-scale testing includes glass column media evaluations, precipitation and filtration tests



Kinetic Column

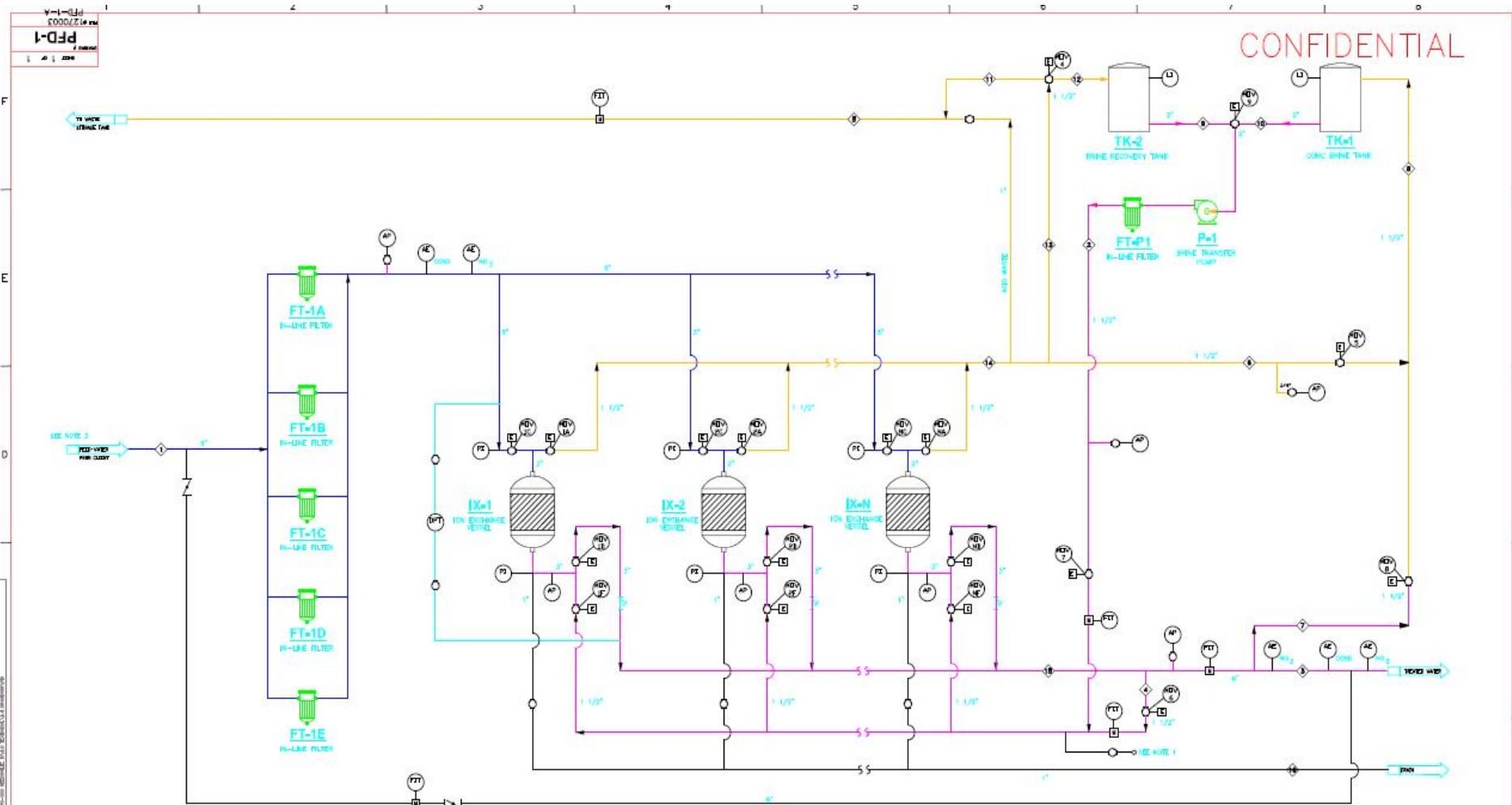


Cross Flow Filtration



Large-Scale Media Pilot

- Media and ion exchange evaluation using columns to several inches in diameter
- Kinetic column testing for media and ion exchange evaluations
- Testing of ion exchange resins and specially formulated selective resins and media
- Cross flow filtration pilots include ceramic, sintered metal and polymeric membranes
- Pilot RO system with 2.5-inch vessels
- Biological reactor pilots for on-site validation



Material Balance

Characteristic		Water Feed	12 wt% Brine	Treated Water	Rinse	Waste Brine	Rinse Recovery	Brine Recovery
		1	2	3	4	5	6	12
Flow	gpm	450	--	--	--	--	--	--
Nitrate	µg/L	--	--	--	--	--	--	--
Iron	µg/L	--	--	--	--	--	--	--
Manganese	gpd	--	--	--	--	--	--	--

Note 1 : Intermittent Flow, Normal rate during operation is shown

GENERAL NOTES:

1. 8% HQ RINSE AS REQUIRED.
2. IX VESSELS, N=4
3. BYPASS TAKEN PRIOR TO FILTRATION.

REV	DATE	DESCRIPTION OF REVISION	APPROVED BY
1	20 NOV 09	INITIAL DESIGN	
2	20 NOV 09	REVISED DESIGN	
3	20 NOV 09	REVISED DESIGN	
4	20 NOV 09	REVISED DESIGN	
5	20 NOV 09	REVISED DESIGN	
6	20 NOV 09	REVISED DESIGN	
7	20 NOV 09	REVISED DESIGN	
8	20 NOV 09	REVISED DESIGN	
9	20 NOV 09	REVISED DESIGN	
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VILLAGE OF NEEDSVILLE

NITRATE REMOVAL
PROCESS FLOW DIAGRAM

HEET 1 of 1

PFD-1

REV 1-1-A

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